



Purification and characterization of α -Galactosidase produced from mutant bacterial strain

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ABSTRACT

An organism producing extracellular α -Galactosidase was isolated from soil and identified as *Bacillus circulans*. An extracellular α -Galactosidase from *Bacillus circulans* has been purified to homogeneity and purity by chromatographic steps, using Sephadex G-100, DEAE-cellulos, and Sephadex G-200. The specific activity of the enzyme was increased approximately 9.5 fold. The molecular weight of the purified enzyme was determined by SDS-PAGE was 81 kDa. The optimum pH and temperature for the purified enzyme were 4.5 and 40°C, respectively. α -Galactosidase is stable over abroad pH rang (3.0-10.0). K_m values for p-nitrophenyl- α -D-galactopyranoside, melibiose, and raffinose were determined 2.00, 50.0, and 97.9 mM, respectively. α -Galactosidase activity was strongly inhibited by Ag^+ and Hg^{2+} metal ions. The enzyme hydrolyzes flatulence causing galactooligosaccharides, viz. raffinose and stachyose present in the soybean

Key words: α -Galactosidase -production- *Bacillus circulans* mutant

INTRODUCTION

α -Galactosidase (EC 3.2.1.22, α -D-galactoside galactohydrolase) is an exo-type glycoside hydrolase that catalyzes the hydrolysis of α -1,6-galactosidic linkages in galactose-containing oligosaccharides such as melibiose , raffinose , and stachyose and in galactomannan, which is commonly found in legumes and seeds. Many sources including plants and microorganisms can produce α -Galactosidase by de nova synthesis depending on environmental conditions and its requirements. Hence bacteria, actinomycetes, yeasts, and fungi were used for enzyme production (Singh and Kayastha, 2013). However, purification to homogeneity and characterization of this enzyme have only been done for a few organisms (Liu et al., 2014).

On the other hand, α -Galactosidase that catalyzes the hydrolysis of simple and complex oligo- and poly-saccharides containing terminal α -D-galactosyl groups and can be found in microorganisms (Ulezlo and Zaprometova, 1982) and plants (Chinen *et al.*, 1981). Several industrial applications of α -D-Galactosidases are known, mainly in food industry. α -D-Galactosidase s are used for hydrolysis of raffinose and stachyose present in leguminous food. (Ohtakara and Mitsutomi, 1987) it can be also used for hydrolysis of raffinose, stachyose, and leguminous polysaccharides present in soybean milk (Kotwal *et al.*, 1998). In sugar industey, α -Galactosidases improve crystallization of sucrose by hydrolysis of raffinose content in molasses during the manufacture process (Linden, 1982). Moreover, they can enhance the bleaching effect in pulp and paper industry (Ratto *et al.*, 1993). The underlying pathology of many human genetic diseases involves molecular changes related to carbohydrate metabolism, largely the complex sugars. Fabry's disease (abnormal sphingolipid metabolism) is due to a deficiency in thermolabile lysosomal α -Galactosidase . Recently, α -D-Galactosidase s are used for medical purposes, e.g. for treatment of Fabry's disease by enzyme replacement therapy (Fuller *et al.*, 2004) or blood type conversion (Olsson *et al.*, 2004).

In the present study we attempted to purification and characterization of α -Galactosidase, in addition its applications

EXPERIMENTAL SECTION

Microorganism sources

The mutant *Bacillus circulans* was isolated and identified from Egyptian soil, the strain was mutant by exposed to gamma irradiation (3.0 kGy).

Production of α -Galactosidase enzyme

The basal growth medium for enzyme production had the following composition: 1g K₂HPO₄, 3g KH₂PO₄, 3g yeast extract, 20g raffinose. The ingredients were dissolved in one liter distilled water. The pH was adjusted to 7.0, for preparation of the inoculum, 1.0 ml of suspension was transferred to 50 ml of the basal medium in a 250 ml Erlenmeyer flask and incubated in a rotary shaker (150 rpm) at 37°C for 24 h. Cultivation was also done in 250 ml Erlenmeyer flask, each containing 50 ml of sterile medium. One milliliter of the inoculum was transferred to the growth medium, then incubated at 37°C in the rotary shaker at 150 rpm., the culture was centrifuged at 5000 rpm for 10 min. and the clear culture filtrate was taken for enzyme assay.

Enzyme assay

α -Galactosidase activity was assayed by measuring the release of p-nitrophenol from chromogenic substrate ((p-nitrophenyl- α -D-galactopyranoside) in citrate phosphate buffer. One unit of α -Galactosidase activity was expressed as the amount of enzyme that liberates 1 μ mol of product (p-nitrophenol) per minute under assay conditions.

Fractionation by salting-out with ammonium sulfate

The method described by Dixon (1953) was used for fractionation of α -Galactosidase by salting-out with ammonium sulfate. In this method, the culture medium was centrifuged at 5000 rpm for 10 minutes in a refrigerated centrifuge to separate the cells. The whole enzyme solution kept in an ice bath then followed by adding solid ammonium sulfate slowly until the required saturation of ammonium sulfate was reached (20, 40, 60, and 80%; w/v). The solution was left overnight at 4°C then centrifuged at 5000 rpm for 25 minutes in a refrigerated centrifuge, each precipitate was dissolved in 10 ml distilled water. The precipitate was dialyzed against distilled water in a cellophane bag (at 4°C) until the water outside the bag gave no precipitation with 1% barium chloride solution. This indicated that the enzyme solution inside the bag became free from excess sulfate. The water outside the bag should be changed several times. For each concentration of ammonium sulfate, the protein content and α -Galactosidase activity were determined in each dialysate.

Gel filtration chromatography

The method described by Wong *et al.* (1986) was used for gel filtration chromatography. In this method, the dialysate of ammonium sulfate fraction was applied to a column (2.6 \times 75 cm) of Sephadex G-100, equilibrated with 0.2 M Na₂HPO₄-0.1 M citric acid buffer solution (pH 5.0), and eluted with the same buffer at flow rate 60 ml/h. The active fractions were pooled and dialyzed against distilled water.

Ion exchange chromatography (DEAE)

The fractions were concentrated and dialyzed against 0.2 M Na₂HPO₄-0.1 M citric acid buffer solution (pH 5.0) then adsorbed on a diethylaminoethyl-cellulose (DEAE-cellulose) column (1.5 \times 40 cm) equilibrated with the same buffer solution. Non-absorbed proteins were washed with the same buffer solution and the adsorbed proteins were eluted with stepwise of NaCl solution (0.1-0.5 M). The column was eluted at flow rate 60 ml/h. The active fractions were pooled and dialyzed against distilled water (Whistler, 1965).

Fractionation by Sephadex G-200 gel filtration

The most active fractions from DEAE-cellulose column were pooled, dialysed as described in previous step and loaded on a (2.5 \times 75 cm) column of Sephadex G-200 equilibrated and eluted with the same buffer solution as described previously. The active fractions were pooled and dialyzed against distilled water.

Electrophoretic techniques

Native-PAGE (without SDS-PAGE and reducing agent) and SDS-PAGE were performed in Bio Rad Mini-Protein II Dual-Slab apparatus according to the method described by Laemmli (1970).

Properties of purified α -Galactosidase

Effect of temperature and pH

The effect of temperature on the activity of the purified α -Galactosidase was determined by standard assay at 30, 35, 40, 45, 50, 55 and 60°C. The α -Galactosidase stability was assessed by incubation of the enzyme for 30 min at the above temperature. The residual α -Galactosidase activity was estimated under standard conditions according to the

method described by (Ohtakara and Mitsutomi, 1984). The effect of pH on enzyme activity was determined using casein as the substrate, which was dissolved in different buffers of pH 3-9. The enzyme stability at various pH values was determined by pre-incubating the enzyme with an equal volume of each buffer for 30 min at 30°C. The residual α -Galactosidase activity was assayed under standard conditions at an optimized temperature of 30°C (Ohtakara and Mitsutomi, 1984)

Effect of metal ions

The purified enzyme was diluted with an equal volume of metal salts (Ag, NO₃, MnCl₂, MgSO₄, HgCl₂ and CaCl₂ solution) with concentrations ranging from 0.1-1mM and incubated for 30min at 30°C. The residual α -Galactosidase activity was assayed under standard conditions.

RESULTS AND DISCUSSION

Four fractions of crude α -Galactosidase produced by mutant *B. circulans* were obtained by four different concentrations of ammonium sulfate (20, 40, 60, and 80 %, w/v). Results obtained was illustrated in Fig.(1). The fraction obtained by 60% (w/v) of ammonium sulfate showed low protein content, high α -Galactosidase activity and specific activity comparing with the crude of α -Galactosidase and other fractions. Therefore, the fraction obtained by 60% (w/v) ammonium sulfate was used for further purification studies.

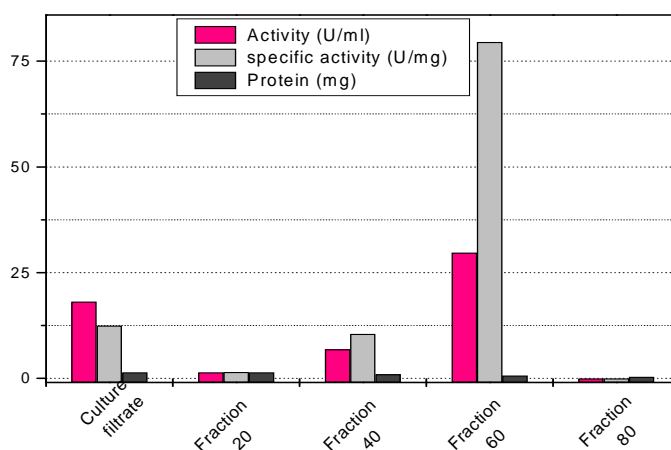


Fig. 1. Protein content, Enzyme activity and specific activity of different fractions of mutant *B. circulans* α -Galactosidase obtained by ammonium sulfate fractionation

In respect of fractionation of α -Galactosidase by salting-out with ammonium sulfate, Wong *et al.* (1986) precipitated α -Galactosidase from *Monscus pilosus* by 50% (w/v) saturation of ammonium sulfate. Moreover, α -Galactosidase produced by *Bacillus stearothermophilus* was precipitated by 50% (w/v) saturation of ammonium sulfate. Rezessy-Szabo *et al.* (2006); Katrolia *et al.*, (2012) isolated thermostable α -Galactosidase from the thermophilic *Thermomyces lanuginosus* CBS 395.62/b. The enzyme was precipitated at 70% concentrated ammonium sulphate, α -Galactosidase produced by mutant *B. circulans* after partial purification with 60% (w/v) ammonium sulfate was applied to a Sephadex G-100. The elution diagram of the enzyme was illustrated graphically in Fig.(2). α -Galactosidase active fractions (from fraction No. 17 to 22) were pooled and concentrated then used for further purification studies. The pooled fractions (from fraction No. 17 to 22) obtained from the previous step (Sephadex G-100) were adsorbed on a DEAE-cellulose. The elution diagram of enzyme purification was illustrated graphically in Fig (3), it was observed that the enzyme was eluted effectively in seven fractions namely from fraction No. 41 to 47. The fractions were pooled, concentrated then used for further purification study. The concentrated enzyme solution obtained from the previous step (DEAE-cellulose) was subjected to the final purification on Sephadex G-200. The elution diagram of the enzyme was illustrated graphically in Fig.(4), it was noticed that the enzyme was eluted effectively in seven fractions namely from fraction No. 9 to 15. The α -Galactosidase active fractions were pooled and dialyzed against distilled water then used for electrophoresis techniques and also for studying the enzyme properties.

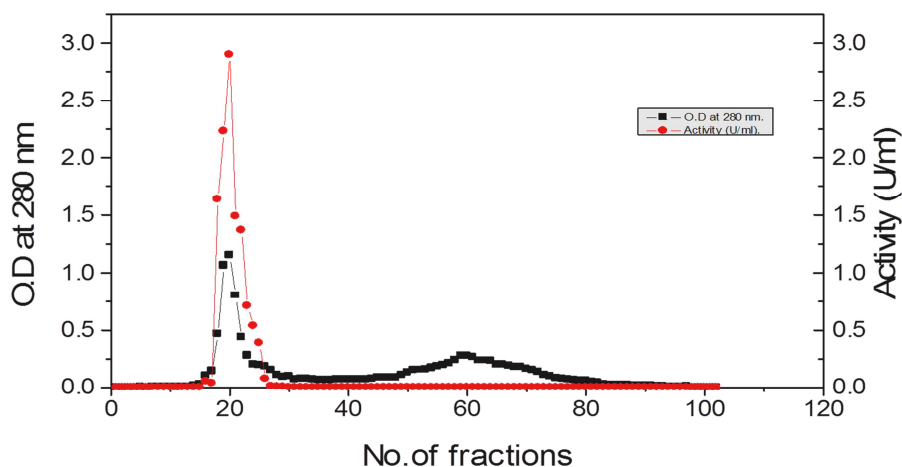


Fig. 2. Elution diagram for purification of mutant *B. circulans* α -Galactosidase obtained by ammonium sulfate precipitation (60% $(\text{NH}_4)_2\text{SO}_4$ fraction) on Sephadex G-100. The column (2.6×75 cm) was equilibrated with 0.2 M Na_2HPO_4 -0.1 M citric acid buffer solution (pH 5.0). Elution was carried out with 500 ml of the same buffer. The flow rate was 1 ml/min and fraction volume 5 ml

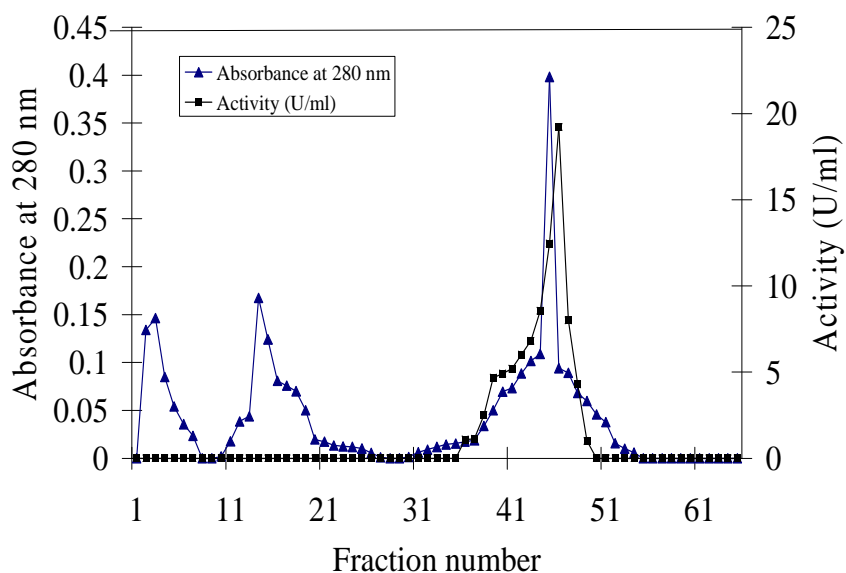


Fig. 3. Elution diagram for purification of mutant *B. circulans* α -Galactosidase on DEAE-cellulose. The pooled fractions (from 17 to 22) obtained from Sephadex G-100 were purified. The column (40×1.5 cm) was equilibrated with 0.2 M Na_2HPO_4 -0.1 M citric acid buffer solution (pH 5.0). Elution was carried out with 500 ml of a linear stepwise of NaCl (0.0-0.5 M). The flow rate was 1 ml/min and fraction volume 5 ml

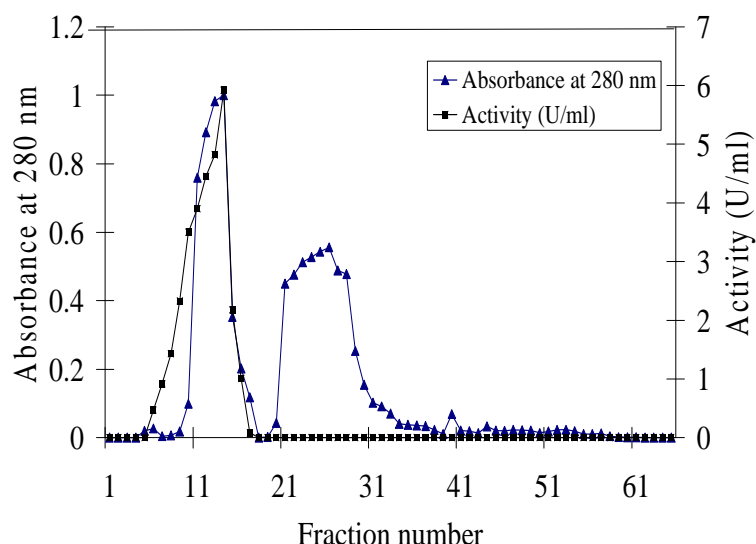


Fig. 4. Elution diagram for purification of mutant *B. circulans* α -Galactosidase on Sephadex G-200. The pooled fractions (from 41 to 47) obtained from DEAE-cellulose were purified. The column (2.5 \times 75 cm) was equilibrated with 0.2 M Na_2HPO_4 -0.1 M citric acid buffer solution (pH 5.0). Elution was carried out with 500 ml of the same buffer. The flow rate was 1 ml/min and fraction volume 5 ml

Total enzyme activity, total protein content, and specific enzyme activity of the proteins at each step of fractionation and purification are summarized in Table (1). The purified α -Galactosidase had a specific activity of 118.27 U/mg protein with 9.5-fold purification. In the present study, the value of specific activity of purified α -Galactosidase (118.27 U/mg protein) was differed from the obtained by Durance and Skura (1985) for *Clostridium perfringens* (1.61 U/mg protein), Talbot and Sygusch (1990) for *Bacillus stearothermophilus* (160 U/mg protein), and Gote *et al.* (2006) for *Bacillus stearothermophilus* (NCIM-5146) (400 U/mg protein).

Table 1. Summary of steps of fractionation and purification of α -Galactosidase from mutant *B. circulans*

Step	Volume (ml)	Total activity (U)	Total protein (mg)	Specific activity (U/mg protein)
Culture filtrate	10000	18190.0	1446	12.500
60% ammonium sulfate fraction	10.00	296.750	3.730	79.650
Sephadex G-100	25.00	265.00	2.500	106.00
DEAE-cellulose	35.00	142.86	1.250	114.29
Sephadex G-200	35.00	92.250	0.780	118.27

5. Electrophoresis

a. Native-PAGE.

The efficiency of the purification process of each step separately (60% ammonium sulfate fraction, Sephadex G-100, DEAE-cellulose, and Sephadex G-200) was evaluated through the Native-PAGE. Native-PAGE was performed under non-denaturing conditions, i.e. in the absence of β -mercaptoethanol and SDS without heating. Gel was conducted using a 12% (w/v) polyacrylamide gel. Fig.(5) shows the resolution patterns of each fraction, obtained data clearly showed that 60% ammonium sulfate fraction (lane 1) consisted of eight bands with R_f value of 0.125, 0.187, 0.387, 0.45, 0.582, 0.75, 0.812, and 0.85. Partially purified protein obtained by Sephadex G-100 (lane 2) consisted of three bands with R_f value of 0.125, 0.387, and 0.812. Semi-final purified protein obtained by DEAE-cellulose (lane 3) consisted of two bands with R_f value of 0.125 and 0.387. Final purified protein obtained by Sephadex G-200 (lane 4) consisted of one band with R_f value of 0.387.

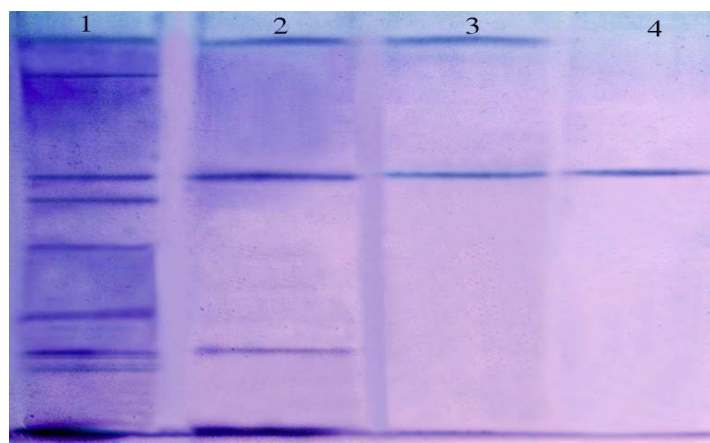


Fig. 5. Native of α -Galactosidase enzyme produced by mutant *B. circulans* at various stages of purification. Analysis performed on a polyacrylamide and stained with Comassie Brilliant Blue R-250. From left to right: Lane 1, 60% ammonium sulfate fraction; Lane 2, partially purified protein obtained by Sephadex G-100; Lane 3, semi-final purified protein obtained by DEAE-cellulose and Lane 4, final purified protein obtained by Sephadex G-200

b. SDS-PAGE

Final purified protein obtained by Sephadex G-200 was subjected to SDS-PAGE. Gel was conducted using a 12% (w/v) polyacrylamide gel gave a single band MW approximately 81 kDa by SDS-PAGE Fig.(6). This single subunit indicating the purity and homogeneity of α -Galactosidase. This molecular weight is slightly differed to those of other reported by Talbot and Sygusch (1990) for *Bacillus stearothermophilus* (73 kDa) and Gote *et al.* (2006) for *Bacillus stearothermophilus* (NCIM-5146) (79.9 kDa). However, the subunit molecular weight of α -Galactosidase from present strain and from other reported strains of the same species (*Bacillus* sp.) ranges between 80 and 84 kDa, suggesting that the gene size could be similar in all these species (Granter *et al.*,1988; Talbot and Sygusch,1990; Fridjonsson *et al.*,1999; and Gote *et al.*,2006)

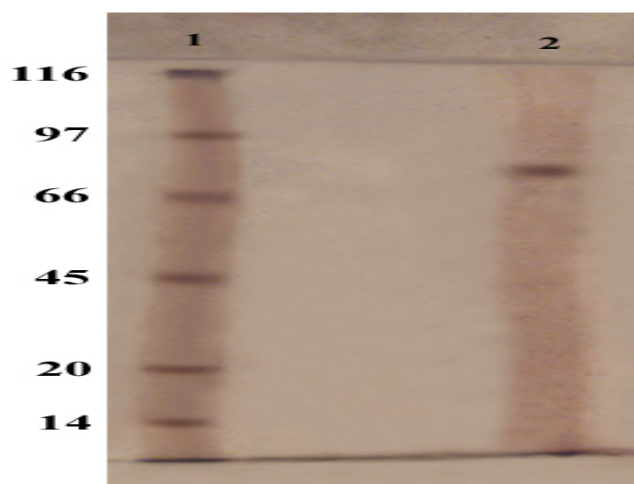


Fig. 6. SDS-PAGE of α -Galactosidase enzyme produced by mutant *B. circulans*. Analysis performed on a polyacrylamide and stained with silver staining technique. From left to right: Lane 1, standard molecular weight markers (β -Galactosidase, 116; phosphorylase b, 97; bovine serum albumin, 66; ova albumin, 45; soybean inhibitors, 20; and α -lactalbumin, 14 kDa) and Lane 2, final purified protein obtained by Sephadex G-200

Properties of purified α -Galactosidase

a. Effect of pH

The aim of the present experiment was to find out the pH value at which α -Galactosidase exhibits its optimum activity. In this respect, different buffers with various pH values, namely citrate buffer (pH 3.0-6.0) and citrate-phosphate buffer (pH 4.0-7.0) were used. In all reaction mixtures prepared, the same amounts of substrate and buffers were added, but each was adjusted at a specific pH value. The reaction mixtures were incubated at 40°C for 30 min. Thereafter, the reaction was stopped and the released glucose was measured. Results obtained are presented as enzyme activity (U/ml) in Fig.(7). The present results indicated that the enzyme activity in citrate-phosphate buffer was the best suitable for enzyme activity because the highest values of α -Galactosidase activity (6.2 U/ml)

were recorded with this buffer followed by citrate-buffer (5.8). From these results, pH 4.5 seems to be the most suitable pH for the enzyme activity. The same findings were observed by Wong *et al.* (1986) who showed that α -Galactosidase activity of *Monococcus pilosus* assayed at 40°C in citrate-phosphate and acetate buffers showed an optimum pH at 4.5-5.0. On the other hand, the optimum pH of enzyme activity from *Aspergillus saitoi* was found at a wide range 4.0 to 8.0 (Sugimoto, and Van-Buren, 1970). Purified α -Galactosidase from *Bacillus stearothermophilus* (NCIM-5146) exhibited maximum activity (more than 70%) in the pH range 5.5-8.0 with optimum at 6.5-7.0

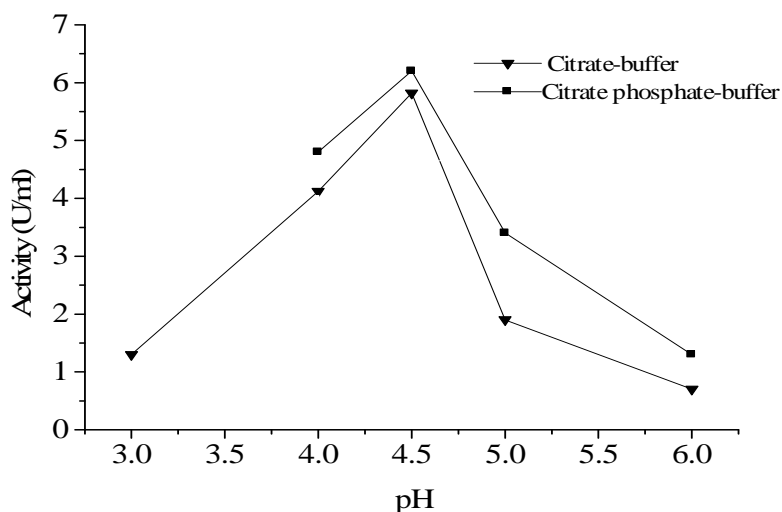


Fig. 7. Effect of pH on the activity of purified mutant *B. circulans* α -Galactosidase

b. Effect of temperature.

The enzyme activity was assayed under the standard conditions, purified enzyme incubated 30 min at pH 4.6 at various temperatures (30, 40, 50, 60, 70, and 80°C) Fig.(8). The enzyme showed maximum activity at 40°C, after this degree a decrease in activity was observed. In general, the optimum temperature for most α -Galactosidase is in the range of 37-40°C (Ulezlo, and Zaprometova, 1982).

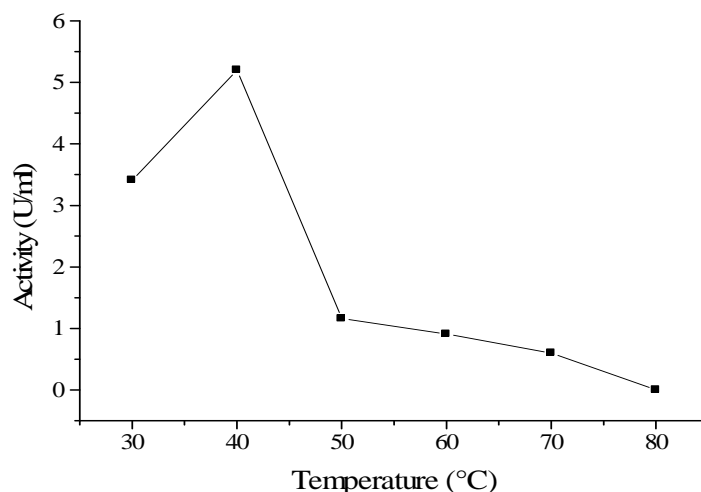


Fig. 8. Effect of temperature on the activity of purified mutant *B. circulans* α -Galactosidase

c. Effect of time.

The effect of incubation time at 40°C on α -Galactosidase activity was examined to establish the assay procedure. The enzyme assay mixture was incubated for 10, 20, 30, 40, 50, and 60 minutes. The results obtained were collected and illustrated in Fig.(9). The results showed that the enzyme activity increased linearly with the time increase and

reached the maximum after 30 min at 40°C. The results also showed that the hydrolysis of melibiose reached its maximum after 30 min of incubation. Incubation of enzyme mixture for more than 30 min did not influence the enzyme activity.

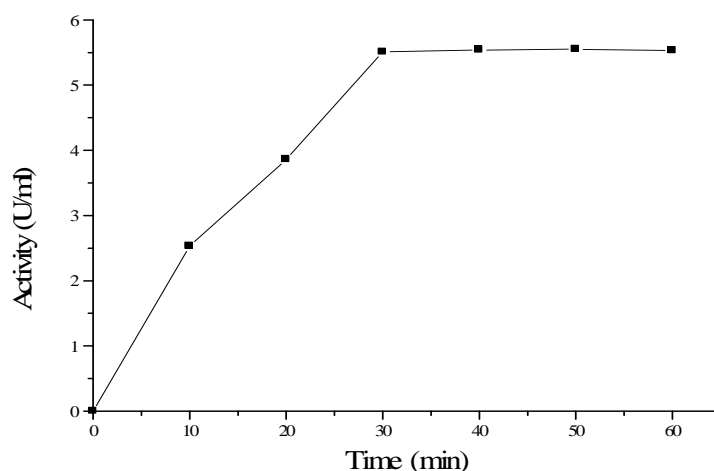


Fig. 9. Effect of time on the activity of purified mutant *B. circulans* α -Galactosidase at 40°C d. pH stability

In this experiment, identical purified enzyme in 0.2 M citrate-phosphate buffer at pH values ranging from 3.0 - 7.0 were incubated at 40°C for 24 h. Thereafter, the pH value of the purified enzyme was directly readjusted to pH 4.5 and added to the mixture containing the substrate then the enzyme activity was determined. Results obtained were presented in Fig.(10). The present results indicated that the enzyme was stable around pH 3.5 at 40°C for 24 h. The same findings were observed by Wong *et al.* (1986) who found that the α -Galactosidase of *Monascus pilosus* was stable between pH range 3.0-8.0. On the other hand, Rezessy-Szabo *et al.* (2006) reported that the *Thermomyces lanuginosus* CBS 395.62/b α -Galactosidase is stable for at least 24 h at 55 °C in the pH range 6.4-8.0.

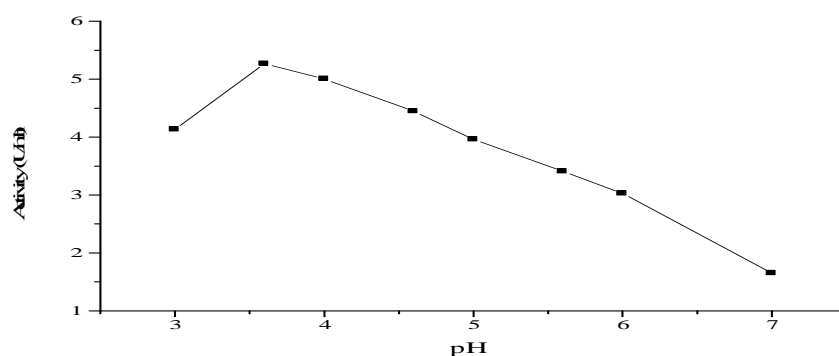


Fig. 10. Effect of pH on the stability of purified *B. circulans* α -Galactosidase incubated at 40°C for 24 h

e. Thermal stability

This experiment was carried out to investigate the heat stability of the purified enzyme (Liu, 2014). Purified enzyme was heated in water bath with different temperatures (30-60°C) for different periods of time up to one hour. Thereafter, the tubes were then rapidly cooled and assayed for α -Galactosidase activity using standard procedures. α -Galactosidase was stable at 30 and 40°C at different time limits as shown in Fig.(11). The residual activity was decreased to 10.22% when the enzyme was stored at 60°C for 30 minutes and completely distorted at 60°C for 40 minutes.

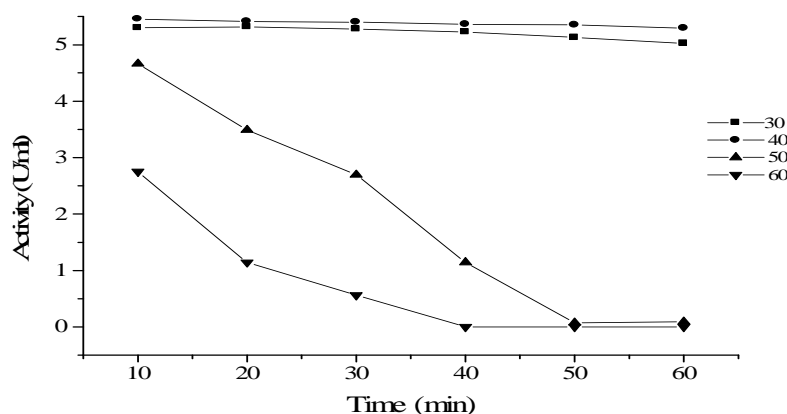


Fig. 11. Effect of temperature on the stability (thermal stability) of the purified mutant *B. circulans* α -Galactosidase

Metal ions and EDTA

The effect of different concentrations of metal ions (AgNO_3 , MnCl_2 , MgSO_4 , HgCl_2 , and CaCl_2) and EDTA on the α -Galactosidase activity is shown in Fig.(12), α -Galactosidase was strongly inhibited by Ag^+ and Hg^{2+} metal salts, while EDTA did not affect the α -Galactosidase activity. These findings were similar to that obtained by Gote *et al.* (2006) and Wong *et al.* (1986) for *Monascus pilosus* and *Bacillus stearothermophilus* (NCIM-5146), respectively. The inhibition by silver ions may be attributed to their reaction with the carboxyl group or histidine residues, and that by mercury ions may be attributed to their binding of thiol group of the enzyme.

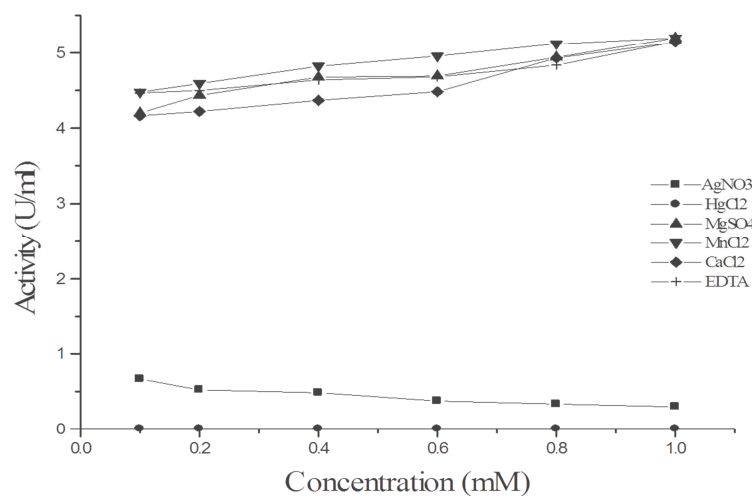


Fig. 12. Effect of different concentrations of metal ions and EDTA on the activity of purified α -Galactosidase

CONCLUSION

After studying the properties of α -Galactosidase enzyme was fixed at a temperature of 40°C and also had the highest activity at pH 4.5. Then when estimated K_m and V_{max} found that the enzyme was active in the presence of Ag^{+2} and Hg^{+2}

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